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CAMBIOR USA, INC.

August 2, 1991

Mr. Geoffrey Shaw
Inspiration Mining Company, Inc.
P. O. Box 70718
Las Vegas, NV 89170

RE: Mining Claims, Mohave County, Arizona

Dear Mr. Shaw:

Thank you for writing to Mr. Louis Gignac regarding your mining claims in Mohave County, Arizona.

Cambior has reviewed the material you submitted to us. We regret that presently we are unable to respond favorably to your properties.

Thank you for contacting Cambior as a potential partner in developing your mineral properties. We wish you success in your endeavors.

Sincerely,

CAMBIOR USA, INC.

Michel Drouin /lat
Michel Drouin
Exploration Manager

MD:lat

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702-786-5189 Fax 702-786-4549

INSPIRATION MINING COMPANY, INC.
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CAMBIOR, INC. .
1075,3RD AVE. EAST. P.O. BOX 999,
VAL D OR QUEBEC CANADA J9P 6M1 2

ATTN. MR. LOUIS P. GIGNAC

SOME TWO YEARS AGO, THIS COMPANY LOCATED IN EXCESS OF 2000 ACRES OF MINING CLAIMS IN MOHAVE COUNT ARIZONA. THIS WAS DONE AFTER SEVERAL RANDOM TESTS THROUGHOUT THE AREA INDICATED THE PRESENCE OF GOLD IN THE ALLUVIAL DEPOSIT.

WE THEN PROCEEDED TO TAKE 140 SAMPLES FROM ONE 80 ACRE AREA TO A DEPTH OF 15 FEET, AND SUBJECTED THESE SAMPLES TO MANY METHODS OF GOLD EXTRACTION. ALTHOUGH THIS IS A GRAVEL TYPE MATERIAL AND CONTAINS A SMALL AMOUNT OF FREE GOLD WE HAVE FOUND THAT SUFFICIENT QUANTITIES OF GOLD CANNOT BE RECOVERED BY GRAVITY SEPARATION.

TWO YEARS OF EXTENSIVE TESTING HAS SHOWN US THAT THE GOLD CAN BE ECONOMICALLY AND PROFITABLY RECOVERED BY OXIDIZING THE ORE WITH OZONE AND LEACHING IT WITH A 1 PERCENT SOLUTION OF POTASSIUM CYANIDE. THIS IS DESCRIBED IN MORE DETAIL IN THE ENCLOSED FLOW SHEET. ALSO ENCLOSED IS OUR CHEMISTS RESUME.

AVERAGE RECOVERY HAS BEEN 0.25 AU. PER TON OF 1/4 MINUS SCREENED ORE. THERE IS ABOUT A 10 PERCENT OVERBURDEN.

INSPIRATION MINING IS A SMALL NEVADA CORPORATION, AND AT THIS STAGE IS NOT IN THE FINANCIAL POSITION TO BUILD A MILL TO PROCESS THE ORE.

WE ARE THEREFORE SEEKING A MINING COMPANY WITH EXPANSION FUNDS AVAILABLE WHO WOULD BE INTERESTED IN ENTERING INTO A BUSINESS ARRANGEMENT WITH US AND PLACING THE PROPERTY INTO PRODUCTION.

SHOULD THIS PROPOSAL APPEAR ATTRACTIVE TO YOU, WOULD YOU PLEASE CONTACT THE UNDERSIGNED FOR FURTHER INFORMATION.

SINCERELY,

G. Shaw.

GEOFFREY SHAW

NEVADA LABORATORY

M E M O R A N D U M

Date : June 8, 1991
From : J.L. Cockrell
To : Geoff and Jack
Subject : Possible flow sheet for processing ore

These notes refer to a drawing on a separate sheet labelled "Flow Sheet".

1. HOPPER: There is a notation '1/4" Grizzly'. This grizzley could well be a screen plant on the property with the processing plant located at a more convenient or safe location. The designation of 1/4" screen size is tentative. More research will be made to determine the optimum screen size.

2. IMPACT GRINDER: This refers to any type of impact or attrition grinder. A common one, and a satisfactory one is the "Hammer Mill". There are others, and the decision is an economic one.

3. AIR CLASSIFIER: This is commonly a cone into which the dust from the mill passes in such a way that a centrifugal motion is imparted. A suitable fan is provided such that an optimum air speed is achieved which will result in all particles less that 100 mesh will flow out of the top of the classifier and all particles greater than 100 mesh will pass through the device provided at the bottom of the classifier to return this oversize material to the mill for further attrition.

4. OXIDIZING LEACH: This is a batch leach in which the ground ore is treated to a severe oxidizing environment for a period of time. At the present, the plan is to use pure ozone dissolved in water. The time is presently set at 12 hours. Further research will be done to optimize the leach time. After the allotted time, the ore is separated by a suitable filter, the ore is transported to another tank, or series of tanks for treatment as described in (7) below. The liquid is passed through ion exchange columns as described in (6) below. The liquid stripped of any contained metal is returned to the oxidizing leach tank for treatment of a new batch of ore. It is possible that further research and engineering will make possible a method for continuous processing at this step.

5. FILTERS: The flow sheet calls for filters after the two leaches at (4) and (7) to separate the ore from the leach fluids. This may well be do by a suitable centrifuge depending on the economics. In each case, the ore must pass to a new location and the liquid must be returned for make up and re-use.

6. ION EXCHANGE: These are shown on the diagram as single columns. In practice they will consist of several columns of appropriate

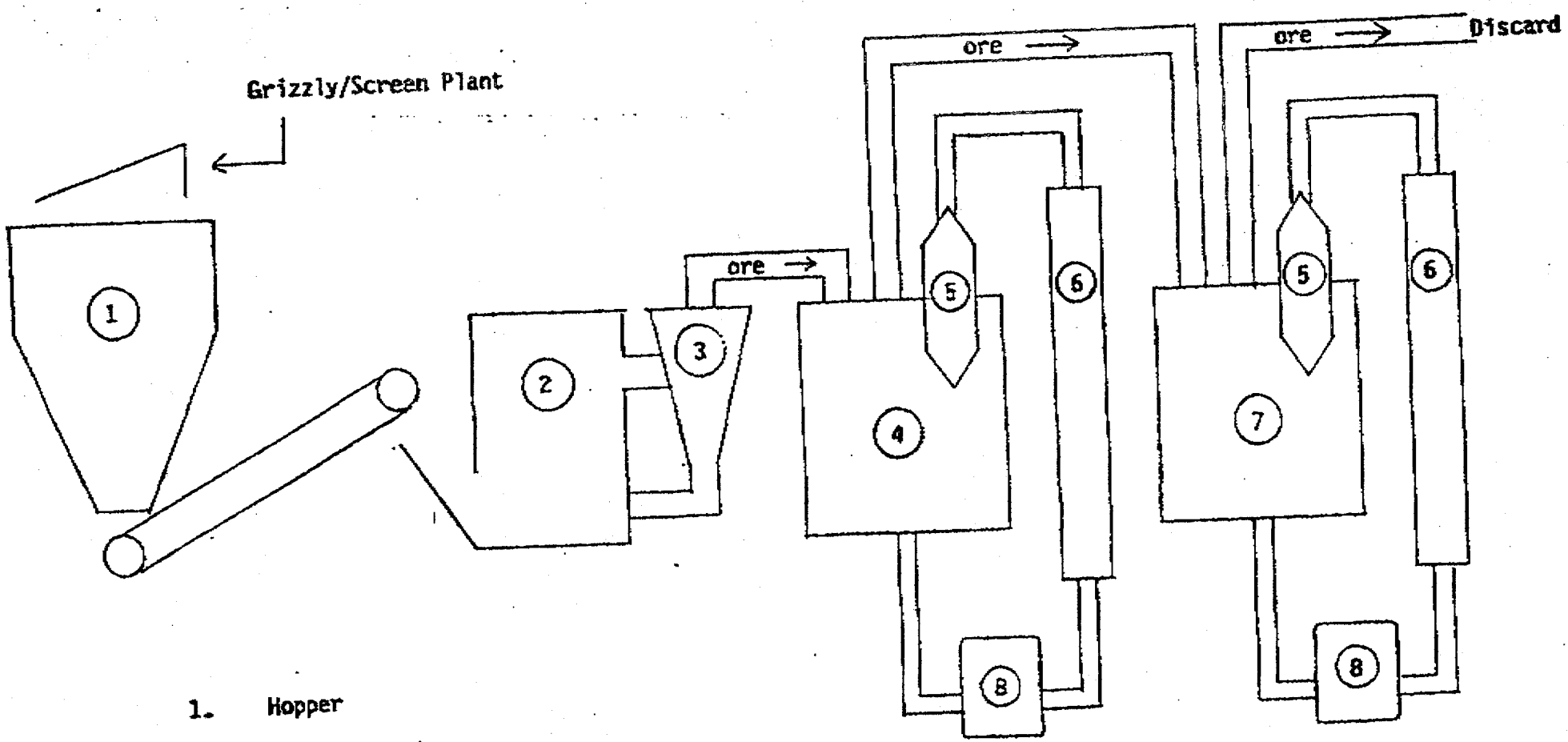
Memo to accompany Flow Sheet

length, and packed with an appropriate resin to strip the leach solution of its metal content. The liquid is introduced from the filter into the first column. It percolates down through the resin beads and passed out the bottom. It is then passed through a second and perhaps a third column and then to a make-up tank and finally returned to the appropriate leach tank to process a new batch of ore.

7. COMPLEXING LEACH: This is a batch leach in which the ore treated to the oxidizing procedure is subjected to a leach solution in which there is a mild oxidizing agent and a complexing agent. The most common complexing leach, and one which works well on this ore, is the cyanide leach. In this case, the leach solution typically consists of a 1% solution of potassium cyanide, or sodium cyanide in water at a pH of about 10 and into which air is dissolved. In this case, the oxygen of the air serves as the oxidizing agent, and the cyanide anion serves as the complexing agent. There are a number of others. To avoid the problems of the toxicity of cyanide, we could use dissolved chlorine as the oxidizing agent and the chloride anion as the complexing agent. In this case, the complex species will be sodium aurochloride and the coordination number will be 4. This makes the anion complex $AuCl_4$. An appropriate ion exchange resin will be packed in the series of ion exchange columns which follow these leach tanks. Also, further research and engineering may well make this a more automatic process.

8. MAKE-UP TANKS: After the leach solutions have been stripped of metal content by passing through the appropriate ion exchange columns, they are essentially returned to their original chemical content, partially diminished by their reactions with the metals in the ore. They are brought back to optimum strength in these make-up tanks. By this method, there is no need to discharge the leach solutions, greatly simplifying the possible pollution and other regulatory problems.

FLOW SHEET



1. Hopper
2. Impact Grinder
3. Air Classifier
4. Oxidizing Leach
5. Filter
6. Ion Exchanger
7. Complexing Leach
8. Make-up Tanks

RESUME

James L. Cockrell

VITAL STATISTICS:

Born: April 22, 1918, at Tulsa, Oklahoma
Married, four grown children.
Present Address: 5724 Caladium Dr., Dallas, TX 75230
Health: Good

EDUCATION:

High School: Public Schools, Tulsa, Oklahoma

University: 1935-1939 University of Illinois: Major Chemistry
1939-1940 University of Oklahoma: B.S. (Geology)
1940-1941 University of Tulsa: Graduate Program (Masters work on the subject, "Correlation of the Oolagah Limestone with Unnamed Sandstones in Northeast Oklahoma. Taught mineralogy as Asst. Professor.)

MILITARY SERVICE:

1941-1945 1st Armored Division, European Theater of Operations. Highest rank, Captain.

WORK EXPERIENCE:

1945-1965 Ross-Martin Company, Tulsa, Oklahoma. Stockholder, Board of Directors, Vice-President in charge of Research and Development.

Major Activities:

1. Worked with the Lithographic Technical Foundation in developing some of the procedures of modern offset lithography.

2. Helped develop some of the procedures of modern full-color photography and printing.

3. Applied Operations Research:
   a. Linear Programming to optimize inventory levels and reorder quantities and improve stock-outs and lower unit prices.

   b. Developed systematic records control and disposal for major companies.

4. Designed geological sample and record-keeping system for major oil companies.

5. Supervised and analyzed transition periods changing operations from hand methods to computers.

1966-1970 General Disposables, Inc., Dallas, Texas. Stockholder, Board of Directors, Vice-President in charge of Research and Development.

Major Activities:

Participated in the development of non-woven fabrics for use in surgery, clean rooms and general purpose disposable clothing.

1971-1979 Consulting Geologist:

1. Exploration for minerals - clay, copper, lead, zinc, fluorspar, gold and silver.

2. Supervised procedures used in mills at Crested Butte, Colorado and Pearce, Arizona.

1981-Present Consulting Geologist

1. Supervised Research at Texas Research and Development Laboratories, Dallas. Included research in extraction methods for recovery of precious metals from ores and concentrates.

2. Retained as consultant on methods of recovery of heavy oil underneath Great Salt Lake. This was for Northlake Industries, Ogden, Utah who had a "farm-out" of the deposit from the owners, AMACO. Continued private research on recovery of heavy oil in conjunction with Robert E. Fearon of Tulsa, Oklahoma.

3. Supervised mining and milling activities at Como, Colorado and Idaho Springs, Colorado.

4. Developed non-toxic leach systems for Dav-Tex, Inc. of Grand Junction, Colorado.